

Synthesis of High Specific Surface Lithium ion Sieve Templated by Bacterial Cellulose for Selective Adsorption of Li⁺

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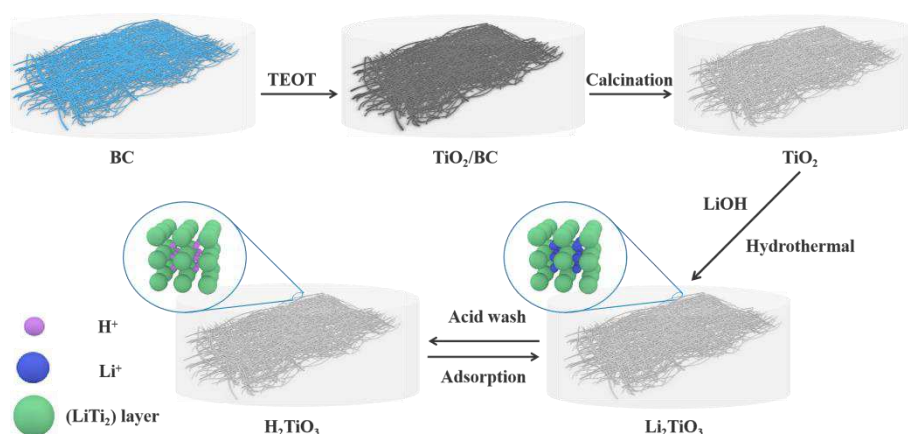
ipSynthesis of high specific surface lithium ion sieve templated by

bacterial cellulose for selective adsorption of Li^+

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Graphical Abstract



Lithium ion sieve templated by bacterial cellulose for selective adsorption of Li^+

Abstract

In recent years, the lithium market has ushered in a golden period of development. With the development of batteries, ceramics, glass, lubricants, refrigerants, the nuclear industry and the optoelectronics industry, the demand for lithium has grown rapidly, and continuous mining has led to scarcity of land resources. On the other hand, due to the rich lithium resources in sea water and salt lake brines. How to selectively adsorb and separate lithium ions from seawater and salt lake brine has attracted more and more scholars' attention and research. Lithium ion sieve stands out because of its excellent performance of specific adsorption and separation of lithium ions. This article reports the preparation of mesoporous TiO_2 and LiOH hydrothermal reaction using bacterial cellulose as a biological template. After calcination at 600°C , spinel lithium titanium oxide Li_2TiO_3 is formed. H_2TiO_3 was obtained by eluting the precursor with HCl eluent. FT-IR, SEM and XRD were used to characterize Li_2TiO_3 and H_2TiO_3 . The adsorption performance of H_2TiO_3 was

24 studied through adsorption pH, adsorption kinetics, adsorption isotherms, competitive
25 adsorption and so on. The results show that H_2TiO_3 is a single layer chemical
26 adsorption process, which has a good adsorption effect on lithium ions at pH 11.0,
27 with the maximum adsorption capacity can reach $35.45 \text{ mg}\cdot\text{g}^{-1}$. The lithium ion sieve
28 has selective adsorption to Li^+ , and its distribution coefficient is $2242.548 \text{ mL g}^{-1}$. It
29 may be predicted that the lithium-ion sieve prepared by biological template has a
30 broad application prospect.

31 **Keywords:** Lithium ion sieve; Bacterial cellulose; Hydrothermal method; Titanium;
32 Selective adsorption

33 **1. Introduction**

34 Lithium is the rarest element among alkali metals(Zeng et al. 2018). It is the
35 lightest silver-white metal with strong chemical activity, can synthesize inorganic and
36 organic compounds of lithium with various elements. Lithium and a variety of metals
37 constitute light alloys, wear-resistant alloys, etc. Al-Li and Mg-Li alloys will become
38 new structural materials for the next generation of aerospace industry. Lithium
39 resources in China are mainly distributed in Qinghai-Tibet Plateau, Xinjiang, Inner
40 Mongolia, Sichuan and Jiangxi, accounting for 25.6 % of the world's lithium reserves,
41 ranking second in the world(DING et al. 2018). Among them, salt lake brine lithium
42 resources are the main form of lithium resources in China, accounting for about 85 %
43 of the total proved lithium reserves in China(Liu et al. 2021). Therefore, it is very
44 important to study how to transform lithium extraction technology and extract lithium
45 efficiently from Salt Lake brine(Argurio et al. 2019). At present, there are many
46 known methods for adsorption and separation of lithium Li^+ from salt lake brine. For
47 example, precipitation method(Song et al. 2017), electrochemical method(Romero et
48 al. 2018), solvent extraction method(Gza et al. 2020; Zhao et al. 2017), ion exchange
49 method(Grágeda et al. 2018; Michel et al. 2018) and so on. Among them, ion-
50 exchange method stands out from many lithium extraction methods because of its
51 simple process, high recovery rate and economic and green advantages(Ma et al.
52 2018). Compared with some natural inorganic minerals and carbon materials(Wen et
53 al. 2017), there is a lack of adsorption selectivity(Lihua et al. 2018) for Li^+ . Lithium

54 ion sieve has the characteristics of selective adsorption of Li^+ because it is first
55 inserted into the precursor by Li^+ and then eluted by eluent(Peng et al. 2019). As the
56 main representative of lithium ion sieves, spinel manganese oxide ion sieves have
57 high specific adsorption for Li^+ after acid elution of precursors. For example, Gao A,
58 Sun Z and others synthesized representative adsorbent $\text{Li}_{1.6}\text{Mn}_{1.6}\text{O}_4$ for lithium ion
59 sieves(Gao et al. 2018). Its maximum adsorption capacity can reach $44 \text{ mg}\cdot\text{g}^{-1}$.
60 Similarly, Yang, Shan Shan, Zhou, Ma Li, Ma Li et al. Through LiOH ,
61 $\text{Mn}(\text{CH}_3\text{COO})_2$, H_2O_2 and ethanol, using sol gel method, hydrothermal method and
62 low-temperature solid-phase method combined with manganese oxide lithium ion
63 sieve made a series of research(Yang et al. 2016). Keiko Sasaki and Qianqian Yu and
64 their colleagues synthesized a lithium ion sieve with microtubule morphology using
65 manganese-oxidizing fungus as biological template by calcination solid-phase
66 bonding. The effect of adsorption capacity at different calcination temperatures was
67 studied. The structural and morphological characterization and adsorption
68 experiments show that the weight fraction of spinel lithium manganese oxide ion
69 sieve also changes with different calcination temperatures, and it will affect its
70 crystallinity, so the choice of calcination temperature directly affects the adsorption
71 capacity of lithium ion sieve(Sasaki and Yu 2015). Song et al. Spinel structure Li_{1+x}
72 $\text{Mn}_{2-x}\text{O}_4$ materials for lithium ion-sieve precursor were synthesized by high
73 temperature solid state method. The results showed that the $\text{Li}_{1.3}\text{Mn}_{1.7}\text{O}_4$ material had
74 the largest adsorption capacity and it reached up to $24.06 \text{ mg}\cdot\text{g}^{-1}$ when the pH value
75 was 12 and the adsorption time was 10 h(Img et al. 2021). However, the current Li-
76 Mn-O ion sieve have the same shortcomings in the process of acid pickling: the
77 appearance of Mn^{2+} in the process of elution causes partial dissolution of the ion
78 sieves, which reduces the repeatability of the lithium ion sieves. On the other hand,
79 the appearance of titanium-based lithium ion sieves compensated for the dissolution
80 of Ti during acid pickling. For example, Shulei Wang, Ping Li and others synthesized
81 $\beta\text{-Li}_2\text{TiO}_3$ by hydrothermal method of TiO_2 and $\text{LiOH}\cdot\text{H}_2\text{O}$ (Zhang et al. 2019).
82 Compared with manganese ion sieves, the dissolution rate of Ti is also reduced while
83 Li^+ is highly selectively adsorbed by manganese ion sieves. Cheng-Long Yua,

84 Kazumichi Yanagisawa et al, synthesized pure Li_2TiO_3 nanoparticles by hydrothermal
85 reaction of anatase TiO_2 and $\text{LiOH}\cdot\text{H}_2\text{O}$, and studied the formation of Li_2TiO_3 , the
86 diffusion and insertion mechanism of lithium ions(Garay-Rodríguez et al. 2019).
87 Ramesh et al. Anatase type TiO_2 and Li_2CO_3 were mixed, ground and heated in an
88 alumina crucible at $700\text{ }^\circ\text{C}$ in air to obtain the lithium ion sieve precursor (Li_2CO_3).
89 The measured adsorption capacity of the adsorbent is $32.6\text{ mg}\cdot\text{g}^{-1}$ (Garcia et al. 2018b).
90 Unfortunately, most of the known lithium ion sieves are powdered, which is not
91 conducive to the mass production of ion sieves in practical applications. Therefore,
92 the preparation of mesoporous nanomaterials to synthesize lithium ion sieve is of
93 special significance(Elik et al. 2018). Cellulose is a polysaccharide with a wide
94 coverage and the largest content in nature(Li et al. 2019). Rich content and low price
95 make it naturally attract the attention of scientific researchers in recent years.
96 However, natural cellulose has some impurities such as lignin and hemicellulose,
97 especially the coarse fiber diameter of natural cellulose, which affects the
98 performance of cellulose(Tomer and Malik 2019). With the in-depth of bacterial
99 cellulose (BC) synthesized by microorganisms under different conditions, the
100 chemical structure of BC is the same as that of plant cellulose(Aimar et al. 2019). The
101 difference is that BC has the advantages of higher purity and finer fiber diameter than
102 plant cellulose. Due to the formation of ultrafine network structure of bacterial
103 cellulose and the "nano-effect", bacterial cellulose has the characteristics of high
104 water absorption and water retention, high permeability to liquids and gases, high wet
105 strength, and in-situ processing and moulding, especially in wet state. High purity and
106 excellent performance can be widely used in many fields.

107 As far as we know, there is no report about the preparation of Li_2TiO_3 by
108 hydrothermal reaction using bacterial cellulose as template. Thus, in this research, We
109 first proposed using BC as a template to form titanium dioxide mesoporous membrane
110 on the substrate. Then, the precursor of Li_2TiO_3 was preliminarily obtained by
111 hydrothermal method with LiOH (Garcia et al. 2018a). The morphology of the
112 precursor was stabilized by calcination at high temperature and the lithium ion sieve
113 with mesoporous shape was obtained by acid elution. Finally, we also proved the

114 excellent adsorption effect of this lithium ion sieve using bacterial cellulose as
115 template in the adsorption experiment, and expected its application prospects.

116 **2. Experimental**

117 **2.1 Synthesis of the Li_2TiO_3**

118 Bacterial cellulose (BC) hydrogel, titanium ethoxide (TEOT), lithium hydroxide
119 (LiOH). Deionized water was used in all experiments. Hydrochloric acid (HCl) and
120 other drugs used are analytically pure, without the need for further processing and
121 purification. Bacterial cellulose (BC) hydrogel was placed in deionized water for 15
122 min to achieve swelling effect. After freezing with liquid nitrogen and freeze-drying,
123 the bacterial cellulose (BC) aerogel with a network structure was obtained. The
124 bacterial cellulose (BC) aerogel was immersed in titanium ethoxide (TEOT) solution
125 for 2 h. Then, after alternately rinsing with ethanol and ultrapure water for 4 to 5
126 times, it was placed in ultrapure water and mechanically stirred for 2 hours, and the
127 product was repeatedly washed with deionized water. Finally, the bacterial cellulose
128 film material TiO_2/BC wrapped in TiO_2 was obtained after drying in the oven (Zhu et
129 al. 2020). TiO_2 with a weight of 0.826 g was obtained by calcining at 600 °C for 6 h at
130 4 °C/min in a tubular furnace. The TiO_2 was dissolved in 10.45 ml of H_2O with 0.5 g
131 of LiOH. The Li: Ti molar ratio of 2:1, unstable spinel Li_2TiO_3 is obtained after
132 hydrothermal reaction at 180 °C for 18 h. The stable spinel Li_2TiO_3 was obtained after
133 being calcined at 4 °C/min at 600 °C for 6 h in a tube furnace.

134 **2.2 Synthesis of the H_2TiO_3**

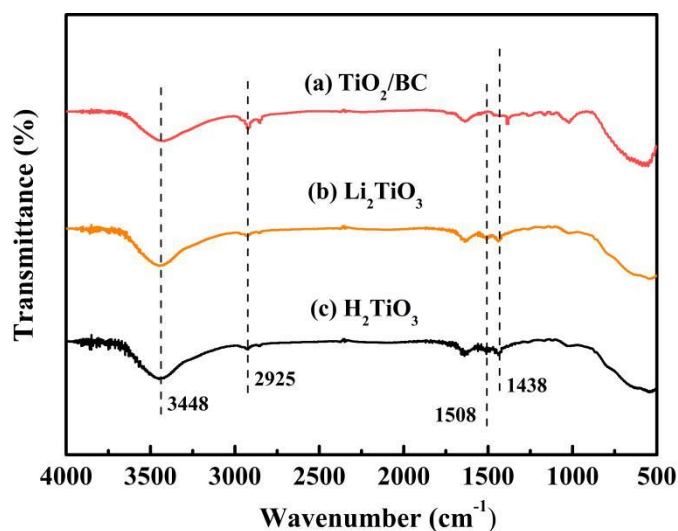
135 Li_2TiO_3 was eluted in the 0.1 mol/L of HCl at 65 °C for 12 h, and then the eluate
136 was changed again to ensure the elution. Finally, the eluted product was washed and
137 filtered with ultra-pure water and dried in an oven at 70 °C. The final product was
138 spinel titanium oxide ion screen. The titanium based lithium ion sieves H_2TiO_3 with
139 high adsorption and specific adsorption for Li^+ were obtained.

140 **3. Results and discussion**

141 **Characterizations of Li_2TiO_3 and H_2TiO_3**

142 In order to analyze functional groups of TiO_2 , Li_2TiO_3 and H_2TiO_3 , FT-IR
143 analysis was performed and presented in Figure 1. Broad peaks at 3448 and 2925 cm^{-1}

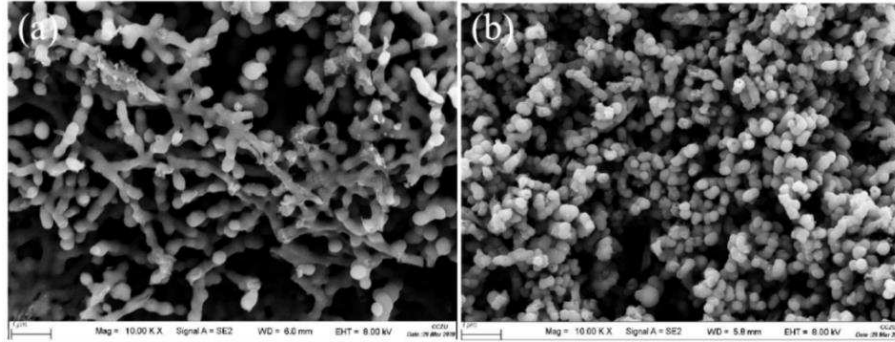
144 were observed for three materials' FT-IR spectra, which can be interpreted as O-H
145 and C-H stretching vibrations, respectively. Among them, OH peak was observed.
146 This peak was due to the isolated O-H bond not participating in the interaction with
147 other hydroxyl groups. In addition, compared with the FT-IR spectra of TiO_2 , the new
148 peaks at 1438 and 1508 cm^{-1} appeared after lithium insertion, which belonged to the
149 characteristics vibration of Li-O-Ti band. It indicates that the precursor (Li_2TiO_3) was
150 formed. In the case of Li_2TiO_3 , the disappearance of peaks at 1438 and 1508 cm^{-1}
151 show successful elution of lithium ions, and the preparation of lithium ion sieve
152 (H_2TiO_3) was completed. As can be seen in the SEM diagram in Figure 2(a), the
153 titania films formed with bacterial cellulose as template feature pronounced high pore
154 volume network structure. After the hydrothermal calcination with LiOH, the films
155 become denser with crystals grow and aggregate, resulting in the formation of spinel
156 Li_2TiO_3 (Figure 2b). The nitrogen sorption data of H_2TiO_3 showed a BET surface area
157 of 27.4006 m^2/g . Based on the adsorption desorption isotherm of nitrogen (Figure 3)
158 shows that the pore structure in the material is consistent with the results of SEM. It
159 can further be inferred that bacterial cellulose as template is effective.



160

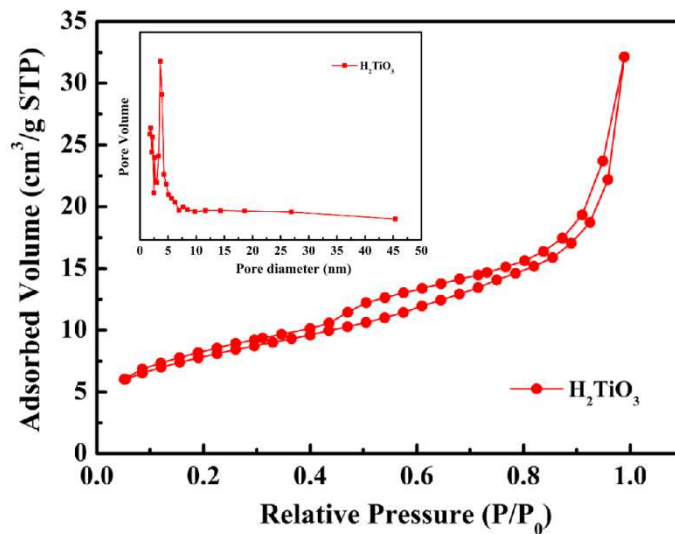
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Fig. 1 (a) FT-IR spectra of TiO_2/BC ; (b) Li_2TiO_3 ; (c) H_2TiO_3



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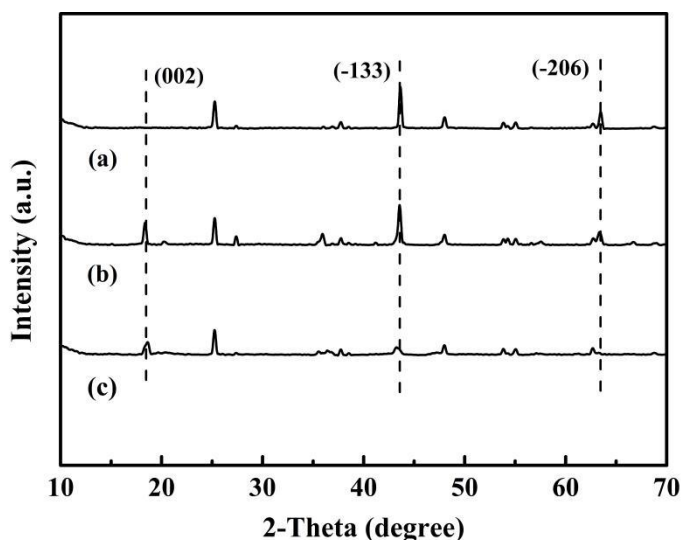
Fig. 2 (a) SEM image of TiO₂/BC; (b) SEM images of Li₂TiO₃.



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165
166

Fig. 3 Nitrogen adsorption-desorption isotherm of H₂TiO₃. Inset showing pore size distributions.

167 As shown in Figure. 4, XRD pattern of the Li₂TiO₃ before calcination, Li₂TiO₃
168 after calcination and H₂TiO₃ were collected at the 2θ angle from 10 to 70°. In the
169 XRD pattern of the Li₂TiO₃, a new diffraction peak at (002) appeared after calcination,
170 which belonged to the growth of (002) diffraction peak needs higher calcination
171 temperature(Gebreslase and Technology 2018). The occurrence of diffraction peaks
172 of (002), (-133), (-206) and (062) can be seen in the Figure 4(b), indicating that Li⁺ is
173 orderedly inserted into TiO₂,which were matched well with the pure monoclinic
174 crystal of Li₂TiO₃(Peng et al. 2019). After eluting, the position of the diffraction
175 peaks can be observed to be about the same, and the diffraction peak of (-133) and (-
176 206) almost disappears, which proves on exchange occurs in Li⁺/H⁺ and the formation
177 of H₂TiO₃ structure.



178

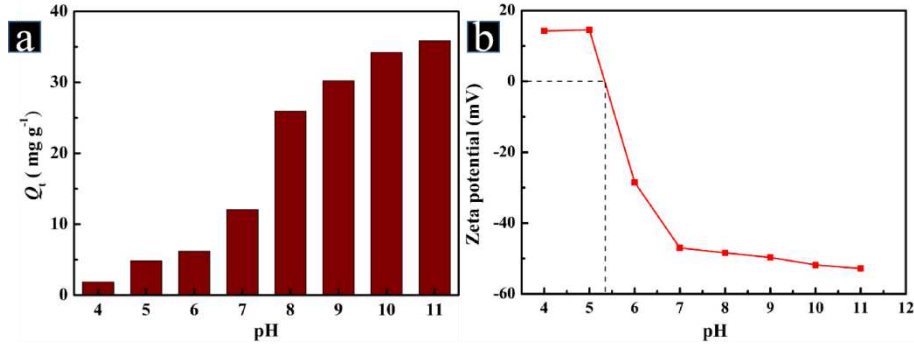
179 Fig. 4 (a) XRD patterns of Li_2TiO_3 before calcination; (b) Li_2TiO_3 after calcination; (c) H_2TiO_3

180 4. Adsorption performance of H_2TiO_3

181 4.1 Effect of pH

182 Here we briefly explore the relationships between Li^+ and its adsorption
 183 mechanism, in which the pH value dominates the study. The pH value is particularly
 184 critical for the adsorption capacity of H_2TiO_3 . As shown in Fig. 5a, with the pH value
 185 increases, the adsorption amount of Li^+ also increases gradually (Sw et al.). It can be
 186 seen that the adsorption of Li^+ is favorable under alkaline condition. In order to avoid
 187 adding more NaOH to adjust the higher pH concentration, thus increasing the effect of
 188 cations in the solutions and considering that the excessively high pH value is not
 189 conducive to mass production in industrial applications. Therefore, the recovery of
 190 Li^+ in this experiment was mainly carried out at pH 11. Fig. 5b shows the zeta
 191 potential test of lithium ion sieve. with the pH increases, the value of the electrostatic
 192 negative charge value on the material also gradually increases. It keeps coincident
 193 with the pH tests results.

194



195
196 Fig. 5 (a) Effect of pH on adsorption capacities (b) Zeta potential measurement of H₂TiO₃

197 4.2. Adsorption kinetics

198 Through the adsorption kinetics experiment, the connection between the
199 adsorption amount (Q_t) and the adsorption time (t) was analyzed. We can see in Figure
200 6, the adsorption curve of the ion sieve adsorbent increased rapidly from the beginning,
201 reaching about 80% of the maximum adsorption capacity at 200 min, then the
202 adsorption curve increases slightly and eventually gradually tends to adsorption
203 equilibrium at about 6 h. The adsorption process of ionic sieve H₂TiO₃ in LiCl
204 solution was fitted by pseudo-first-order kinetic model (PFOKM), pseudo-second-
205 order kinetic model (PSOKM) to explore the adsorption rate constant and mechanism.
206 The fitting equation of the PFOKM and PSOKM as follows:

$$Q_t = Q_e - Q_e e^{-k_1 t} \quad (1)$$

$$Q_t = \frac{k_2 Q_e^2 t}{1 + k_2 Q_e t} \quad (2)$$

207 Where, Q_t (mg.g⁻¹) corresponds to the amount of Li⁺ adsorbed at time t (min) and
208 Q_e (mg.g⁻¹) corresponds to the amount of adsorption at equilibrium. k_1 (min⁻¹) and k_2
209 (g.mg⁻¹.min⁻¹) are the rate constants of the PFOKM and PSOKM, respectively. In
210 addition, the h (mg.g⁻¹.min⁻¹) and $t_{1/2}$ (min) of the PSOKM are listed in the following
211 formulas (3) and (4):

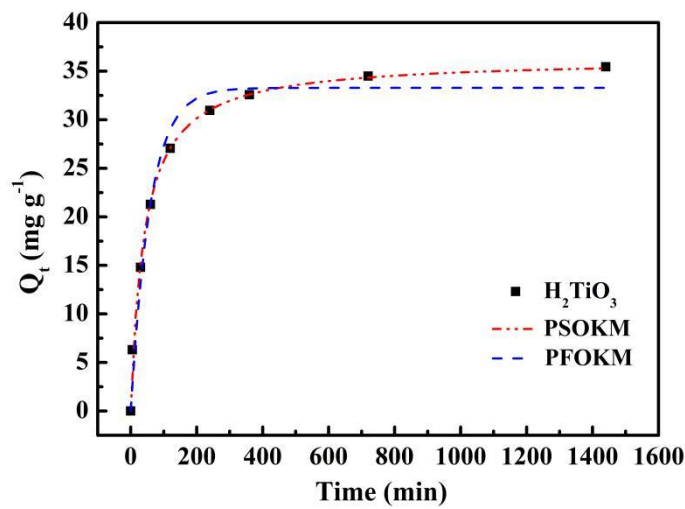
$$h = k_2 Q_e^2 \quad (3)$$

$$t_{1/2} = \frac{1}{k_2 Q_e} \quad (4)$$

212 The kinetic curve of adsorption was fitted by PFOKM and PSOKM. The fitting
213 curve and corresponding parameters are presented in Figure 6 and Table 1,
214 respectively. Obviously, the correlation coefficient of R^2 fitted by PSOKM is larger

215 than the correlation coefficient of R^2 fitted by PFOKM, which better matches the
 216 experimental data.

217 At the same time, the equilibrium adsorption amount calculated based on the
 218 PFOKM and the PSOKM. Compared with the actual values, the results of the pseudo-
 219 secondary dynamics model are closer to reality. Therefore, we believe that PSOKM is
 220 more in line with the adsorption of ion sieve H_2TiO_3 in LiCl solution. This further
 221 illustrates that the adsorption process of Li^+ by H_2TiO_3 is mainly completed under the
 222 chemical action.



223

224 Fig.6 Kinetic data and modeling for the adsorption of Li^+ : Fitting curves of PFOKM and PSOKM

225

Table 1. Kinetic parameters for the PFOKM and PSOKM

Sorbents	$Q_{e,exp} (mg \cdot g^{-1})$	PFOKM			PSOKM		
		$Q_{e,c} (mg \cdot g^{-1})$	$k_1 (min^{-1})$	R^2	$Q_{e,c} (mg \cdot g^{-1})$	$k_2 \times 10^{-2} (g \cdot mg^{-1} \cdot min^{-1})$	R^2
H_2TiO_3	35.45	33.28	0.0172	0.975	36.29	0.068	0.991

226 4.3. Adsorption isotherms

227 By statically testing equilibrium adsorption data and adsorption curves in LiCl
 228 solutions ($100-2000 mg \cdot L^{-1}$), so as to explore the equilibrium concentration and
 229 adsorption amount of the adsorbent in different concentrations of lithium-containing
 230 solutions. Among them, from the curve fitted by Langmuir and Freundlich equation
 231 (Figure 7), the adsorption effect will become higher with the increase of Li^+
 232 concentration. The saturation adsorption capacity of H_2TiO_3 is $35.45 mg \cdot g^{-1}$. The
 233 related isothermal constants are listed Table 2. It is not difficult to see that the

234 correlation parameters of the Langmuir and Freundlich adsorption isotherm models
 235 are $R^2=0.996$ and $R^2=0.978$, respectively. In comparison, the Langmuir isotherm
 236 adsorption model can better match the experimental data, which also corresponds to
 237 the single layer adsorption. This indicates that fitting experimental data with
 238 Langmuir equation is closer to actual data. Hence, the lithium ion sieve is known as
 239 an adsorbent with excellent performance in extracting Li^+ . Experimental data fit via
 240 Langmuir and Freundlich models, which were calculated by Eqs. (5) and (6):

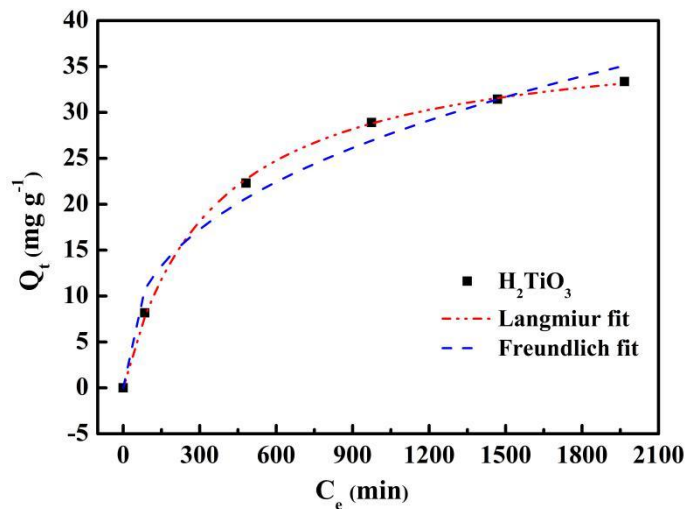
$$Q_e = \frac{K_L Q_m C_e}{1 + K_L C_e} \quad (5)$$

$$Q_e = K_F C_e^{1/n} \quad (6)$$

241 In the formula, Q_m ($\text{mg} \cdot \text{g}^{-1}$) is expressed as the maximum amount of H_2TiO_3 to
 242 Li^+ . K_L ($\text{L} \cdot \text{g}^{-1}$) corresponds to the Langmuir isotherm constant. K_F ($\text{mg} \cdot \text{g}^{-1}$)
 243 corresponds to Freundlich isotherm direction constant, $1/n$ corresponds to the effect of
 244 concentration on the amount of adsorption, R_L is used as a separation factor to identify
 245 the merits of H_2TiO_3 , which the calculation formula of R_L is listed in formula (7):

$$R_L = \frac{1}{1 + C_m K_L} \quad (7)$$

246 In this formula, C_m is explained as the maximum initial concentration of Li^+ .



247

248

Fig.7 Isotherm model fitting of on H_2TiO_3 adsorbing Li^+ .

249

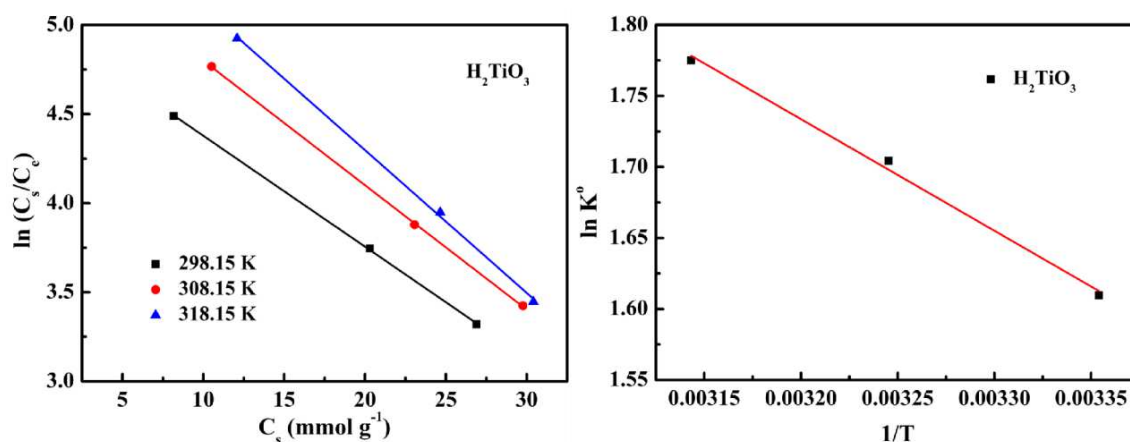
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Table 2. Adsorption equilibrium constants of Langmuir and Freundlich models

Sorbents	Langmuir isotherm model			Freundlich isotherm model		
	Q_m ($\text{mg}\cdot\text{g}^{-1}$)	K_L ($\text{L}\cdot\text{mg}^{-1}$)	R^2	K_F ($\text{mg}\cdot\text{g}^{-1}$)	$1/n$	R^2
H_2TiO_3	38.96	0.003	0.998	2.01	0.38	0.948

252 4.4. Effect of temperature

253 Further, considering the influence of thermal motion characteristics on the
 254 adsorption efficiency. Therefore, we explored the effect of H_2TiO_3 on Li^+ adsorption
 255 at different temperatures (298.15 K, 308.15 K, and 318.15 K) through thermodynamic
 256 experiments. ΔG° is calculated from the Gibbs free energy formula, and the change of
 257 Q_e with temperature was studied (Fig. 8 (a)). ΔH° and ΔS° are calculated by the $\ln K^\circ$
 258 equation, and the change of van't Hoff plot of $\ln K^\circ$ to $1/T$ was studied (Fig. 8
 259 (b))(Zhang et al.). The results of the thermodynamic parameters of the ion sieve are
 260 shown in Table 3. It can be observed that at a temperature of 298.15-318.15K, the
 261 value of ΔG° is maintained at -3.85 to -4.73 $\text{kJ}\cdot\text{mol}^{-1}$, and is always negative. It
 262 indicates that as the temperature increases, the adsorption capacity will gradually
 263 become higher. That is to say, the adsorption of Li^+ is a spontaneous process. At the
 264 same time, ΔH° is always positive, which can be explained as an endothermic
 265 adsorption process, indicating that the Li^+ adsorption effect will increase with
 266 increasing temperature. Hence, we believe that the adsorption of Li^+ on the ion sieve
 267 is a spontaneous endothermic process.



268

269 Fig. 8 Thermodynamic properties of Li^+ on H_2TiO_3 at 298.15, 308.15, and 318.15 K

270

271

Table 3. Thermodynamic parameters for Li⁺ adsorption

<i>Sorbents</i>	ΔH° (kJ mol ⁻¹)	ΔS° (J mol ⁻¹)	<i>T</i> (K)	<i>K</i> ^o	ΔG° (kJ mol ⁻¹)	<i>R</i> ²
H ₂ TiO ₃	6.54	35.31	298.15	5.00	-3.99	0.992
			308.15	5.50	-4.37	
			318.15	5.90	-4.70	

272

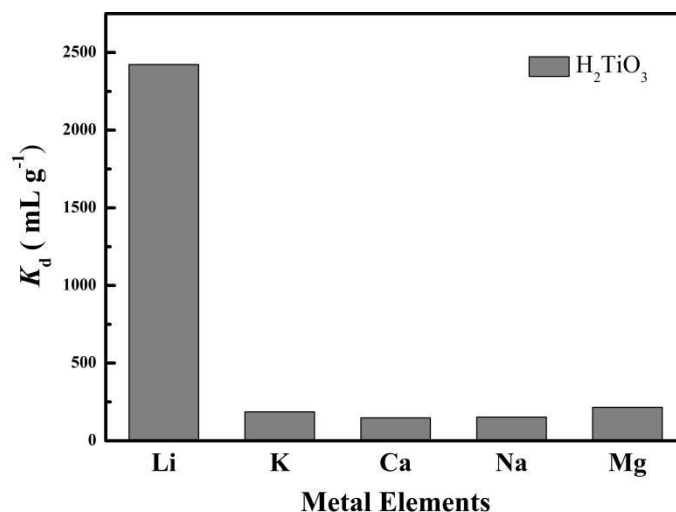
273 **4.5. Selective and reusability tests**

274 Through selective experiments to determine whether H₂TiO₃ has a specific
 275 adsorption selectivity for Li⁺, we simulated salt lake brine for competitive adsorption
 276 experiment, and tested the adsorption performance of H₂TiO₃ to Na⁺, Mg²⁺, K⁺, Ca²⁺,
 277 Li⁺. *K_d* (mL·g⁻¹) is the partition coefficient and *k* as the selectivity coefficient were
 278 used as indicators to evaluate the selectivity of H₂TiO₃. According to the magnitude
 279 of the comparison *K_d* value, the adsorption selection performance of H₂TiO₃ for Li⁺
 280 can be judged. From the experimental results, we can clearly observe that when the
 281 adsorption reaches equilibrium, the adsorption effect and partition coefficient (*K_d*) of
 282 Li⁺ by H₂TiO₃ are several times that of other metal ions. Based on this, it can be
 283 determined that the lithium ion sieve H₂TiO₃ specifically adsorbs Li⁺. The selectivity
 284 of ion sieve for Li⁺ K⁺ Ca²⁺ Na⁺ Mg²⁺ was assessed by distribution coefficient (*K_d*,
 285 mL g⁻¹), which is listed in formula (8):

$$k_d = \frac{C_0 - C_f}{C_f} \times \frac{V}{m} \quad (8)$$

286 In this formula, *C₀* is interpreted as the initial concentration of five ionic
 287 solutions, and *C_f* represents the final concentration of each ionic solution.

288 The industrial feasibility of lithium ion sieve was verified by adsorption cycle
 289 experiment, so that the production cost was minimized. After each adsorption, the
 290 eluent (0.1M HCl) desorbs the adsorbent. Such a process is called a cycle. The
 291 experimental results are shown in Fig. 11. After 5 cycles, the capacity of the
 292 adsorbent remained above 82% of the initial value. All these results confirm that
 293 H₂TiO₃ has a good cycle adsorption potential for Li⁺.



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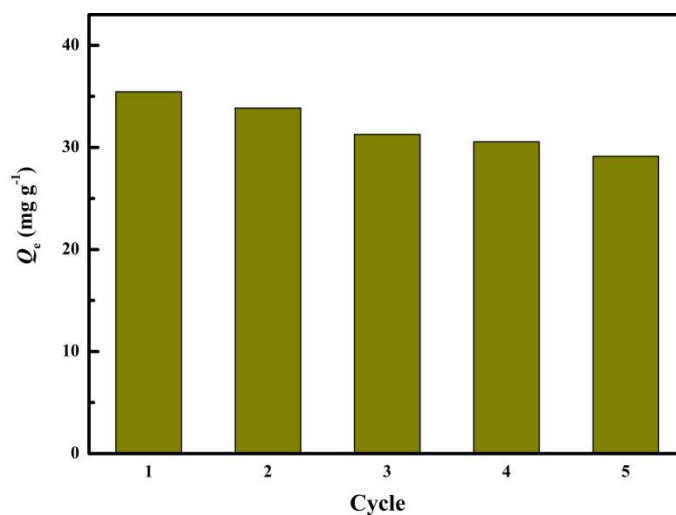
Fig.9 K_d values of H_2TiO_3 for a mixture of Na^+ , Mg^{2+} , K^+ , Ca^{2+} , Li^+

296

Table 4. K_d and k values of H_2TiO_3

Cation	H_2TiO_3		
	C_f ($mg \cdot L^{-1}$)	K_d ($mL \cdot g^{-1}$)	k
Li^+	14.609	2422.548	
K^+	48.059	40.388	0.017
Ca^{2+}	45.961	87.879	2.176
Na^+	47.634	49.670	0.565
Mg^{2+}	44.087	134.121	2.700

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Fig.10 Regeneration of H_2TiO_3 5 cycles.

300 4. Conclusion

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In this study, a lithium ion sieve with bacterial cellulose as a template was successfully prepared and used for the specific adsorption and separation of Li^+ from seawater and salt lake brine. And it shows excellent periodicity and stability in

304 adsorption, elution and circulation experiments. At the same time, using bacterial
305 cellulose as a biological template, the preparation of mesoporous titanium-based
306 lithium ion sieve was realized. Compared with the previous methods of assembling
307 lithium-ion sieve, the ion sieve prepared by using cellulose as biological template not
308 only has a slightly higher adsorption capacity, but also has the mesoporous structure
309 provided by bacterial cellulose, which provides more possibilities for future research.
310 Therefore, we believe that the spinel-type titanium dioxide ion sieve prepared by this
311 method has broad application prospects and is expected to be widely used.

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319 **Declarations**

320 **Conflict of interest**

321 The authors declare that they have no conflict of interest.

322 **Ethical approval**

323 The article does not contain any experiments with human participants or animals
324 performed by any of the authors.

325 **Informed consent**

326 Informed consent was obtained from all individual participants included in the st
327 udy

328 **References**

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