Pyrometallurgy and Electrometallurgy of Rare Earths – Part B: Cell design, construction, rate processes, and unit operation

Muhammad Musaddique Ali Raque (ali.raque@easternengineeringcambridge.onmicrosoft.com)
Eastern Engineering Solutions Inc.

Muhammad Musaddique Ali Raque (ali.raque@easternengineeringcambridge.onmicrosoft.com)
Massachusetts Institute of Technology  https://orcid.org/0000-0001-9157-2589

Short Report

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Abstract

Production of rare earths by metallothermic reduction and its variants is presented in an earlier study and its analysis is performed indicating major type and sequence of reactions. Diagrams required and procedures to establish them are also described. Their role and importance are also described. A comparison is also made to identify parameters of importance. This study is continuation of a previous study in which cell design to extract metals is described. Parameters to design and construct cell (metallothermic and electrothermic) are determined and used. Rate processes (heat transfer, mass transfer, charge transfer and simultaneous processes) occurring inside a cell, its operation for a specific reaction and sequence for a specific metal (Nd) are described. Outline of calculations outlining cell efficiency, output and yield are enumerated for individual (Nd, Ce, Dy) metal. Optimization and method to achieve is described. Procedures to control and production is also described. Here preliminary graphs are presented.

1. Introduction

Essentially, pyrometallurgical processes involves design of furnace for melting, holding, and refining of metal oxides and compounds while electrowinning and electrorefining (after pyrometallurgy) involves design and control of electrochemical cell (room or high temperature) operated by the fundamental principles of current density, its control, distribution, and electromotive force (EMF). Its detail may be found in specialized texts [1–7] and literature [8–11]. This study is continuation of previous study of author [12] on the subject describing extraction and refining of rare earths from their ores by metallothermic reduction. In this area of emphasis is cell design and rate processes (heat, mass, and activity coefficient determination) which lead towards economic production of these metals from their source. Various graphs and carts are presented lying emphasis on the efficient extraction and refining of rare earths. Nd-Fe foundry alloy is taken as example to describe construction and operation of cell. Unit operation including piping and instrumentation diagrams (P&IDs) is described to explain different (Elution and electrowinning) circuits. Lastly, a future outlook is presented to calculate individual efficiency and throughput.

2. Fundamentals

Cell design of rare earth electrowinning process depends on type of metal won (Nd [8], Sm, W, Th, U, Ce, Sc), its quantity required, production rate, type of electrolyte, concentration of metal in electrolyte and flow rate of electrolyte.

3. Cell Design

Cell design primarily consists of outlining parameters of its construction based on its holding capacity. It may be carried out in various ways such as production rate, throughput, efficiency, yield but design based on holding capacity constitutes the simplest. It is presented here.
Consider a typical cell of 5 ton / day. For this, considering rectangular dimensions (as they ease out operation and maximizes yield)

4. Rate Processes

Research progress in development and processing of rare earths may be described following [13, 14]. Density of a typical metal as a function of concentration and temperature is presented by following equation.

\[ \rho = -6.53212 \times 10^{-4} c^2 - 0.06987 c + 1.31265 \times 10^{-5} T^2 - 0.05297 T + 1.69004 \times 10^{-4} cT + 43.14013 \]

**Solubility and dissolution of rare earth oxide in the fluoride melt** [15]

Rare earths in their oxide forms may exhibit solubility and may be dissolved in their oxide and fluoride electrolyte melts.

Nd\(_2\)O\(_3\) solubility in fluoride melts with different NdF\(_3\)-LiF compositions and at different temperatures [15].

**Production of Nd-Fe foundry alloy by the electrolysis of neodymium fluoride**

During the electrolysis of these melts at the electrodes the following reactions are taking place: at the graphite anode. [16]

\[ \begin{align*}
2F^- - 2e & \rightarrow F_2 (\text{gas}) \\
C + 2F^2 & \rightarrow CF_4 (\text{gas}) \\
2Cl^- - 2e & \rightarrow Cl_2 (\text{gas})
\end{align*} \]

at the iron cathode:

\[ \begin{align*}
Nd^{+3} + 3e & \rightarrow Nd \\
Nd + Fe & \rightarrow Nd_2Fe + aNd - \text{low-melting eutectic (T}_m = 640 \degree C)\]
\]

**Production of Nd-Fe foundry alloy by the electrolysis of neodymium oxide**

During the electrolysis of neodymium oxide in fluoride melts at the electrodes the following reactions are taking place at the graphite anode [16]

\[ \begin{align*}
2O^- - 4e & \rightarrow O_2 \\
C + O_2 & \rightarrow CO_2 (\text{gas}) \\
2C + O_2 & \rightarrow 2CO (\text{gas})
\end{align*} \]

at the iron cathode:
Following coefficients are important, must be considered and calculated for effective electrometallurgical operations. Activity coefficients, diffusion coefficients, equilibrium separation coefficients, effective separation coefficients.

Vapor pressure

Cell efficiency

Cell efficiency may be calculated by measuring the concentration of reactant and product species in electrolyte. An excellent study documents these in Cerium [18]. Interested reader is referred to it for further details.

Mass transfer

Mass transfer coefficients, solubility of rare earth oxides in molten fluorides, oxide solubility determinations, oxide solubility diagrams. Prior to the proper oxide solubility determinations and diagram development, the equilibration time for oxide source dissolution, e.g., Dy$_2$O$_3$ and Dy$_2$(CO$_3$)$_3$, was determined. It was determined by adding a certain amount of the oxide source (below solubility limit) and sample analysis thereafter at certain intervals. The time of equilibrium dissolution is measured by noting time at which the analyzed oxide content becomes constant. Below figures (Fig – 5) show the results obtained when Dy$_2$O$_3$ was added to the DyF$_3$-LiF melts at different compositions, i.e., DyF$_3$ (50 mol pct)-LiF (50 mol pct) and DyF$_3$ (20 mol pct)-LiF (80 mol pct), at a working temperature of 1323 K (1050 C). The results showed that in the case of the eutectic composition longer dissolution times than in the equimolar composition are needed, in which case, all Dy$_2$O$_3$ added is dissolved well within 30 minutes.

Diagrams for electrodeposition of Nd from its salts are described below [19]

5. Unit Operations

Unit operations consist of drawing procedures to operate plant, optimize them, making P&IDs, setting them, calculating reactions and their sequences, and calculating efficiencies and throughput.

Piping and Instrumentation Diagrams (P&IDs)

Piping and Instrumentation Diagrams (P&IDs) for rare earths. For a typical 5 ton / day plant, example optimized P&IDs are developed. Example P&IDs for Au processing plants are shown here [20].
Efficiency and throughput

Efficiency and throughput of individual cell comprising of circuits and P&IDs constitutes an important part of the process and an important rare determining step. These must be carefully calculated and will be presented in subsequent studies with details about each and every individual step.

6. Conclusions

Various relations may be used to drive and arrive at optimum relations for efficient electrometallurgical operation of cell for efficient extraction and refining of rare earth metals from their salts. These in turn may depend on various intrinsic factors such as activity, heat, and mass transfer coefficients.

References


**Declarations**

Competing interests: The authors declare no competing interests.

**Figures**

![Figure 1](image)

**Figure 1**

Plot of density as a function of NdF₃
Figure 2

Solubility of rare earth oxide in fluoride molten salts [15]
Figure 3

Dependence of current efficiency for Nd on the cathode current density at temperature of process $t = 750^\circ$C (a) Electrolyte $\text{NdF}_3 - \text{LiF} - \text{BaF}$ (b) Electrolyte $\text{BaCl}_2 - \text{LiCl} - \text{NdF}_3 - \text{LiF}$, (c) Electrolyte $\text{BaF}_2^+ - \text{NdF}_3 - \text{LiF}$ [15].
Figure 4

Vapor pressure as a function of temperature for various rare earth metals (a) Saturated vapor pressure of Tb, Mn and Cr, (b) vapor pressure of other rare earth metals [17]
Figure 5

Dissolution rate of Dy$_2$O$_3$ added to the DyF$_3$-LiF melt in composition: (a) equimolar, and (b) eutectic, (c) Dissolution rate of anhydrous Dy$_2$(CO$_3$)$_3$ added to the equimolar DyF$_3$-LiF melt. Temperature 1323 K (1050 C).
Figure 6

E/Volts vs ref. electrode diagrams [19]
Figure 7

Elution circuit

Figure 8
Electrowinning circuit

Figure 9

Zadra Elution process